

PCT

WORLD INTELLECTUAL PROPERTY ORGANIZATION  
International Bureau



INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification <sup>6</sup> : <b>A23L 1/308</b>		A1	(11) International Publication Number: <b>WO 95/20328</b> (43) International Publication Date: <b>3 August 1995 (03.08.95)</b>
(21) International Application Number: <b>PCT/US95/01001</b>		(81) Designated States: AM, AT, AU, BB, BG, BR, BY, CA, CH, CN, CZ, DE, DK, EE, ES, FI, GB, GE, HU, JP, KE, KG, KP, KR, KZ, LK, LR, LT, LU, LV, MD, MG, MN, MW, MX, NL, NO, NZ, PL, PT, RO, RU, SD, SE, SI, SK, TJ, TT, UA, UZ, VN, European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG), ARIPO patent (KE, MW, SD, SZ).	
(22) International Filing Date: <b>26 January 1995 (26.01.95)</b>		Published <i>With international search report.</i>	
(30) Priority Data: <b>08/187,971 28 January 1994 (28.01.94) US</b>			
(71) Applicant: <b>FMC CORPORATION [US/US]; 1735 Market Street, Philadelphia, PA 19103 (US).</b>			
(72) Inventors: <b>McGINLEY, Emanuel, J.; 57 Kirby Drive, Morrisville, PA 19067 (US). KRAWCZYK, Gregory, R.; 8 Colonial Avenue, Princeton Junction, NJ 08550 (US). SELINGER, Edward; 329 Flint Road, Langhome, PA 19047 (US).</b>			
(74) Agent: <b>FELLOWS, Charles, C.; FMC Corporation, 1735 Market Street, Philadelphia, PA 19103 (US).</b>			
(54) Title: <b>COPROCESSED PARTICULATE BULKING AND FORMULATING AIDS</b>			
(57) Abstract <p>A composition that is a composite of cellulose and a surfactant. The composite is made by the process of coprocessing the cellulose with a surfactant. The composite can be used as a bulking agent in intermediate and high moisture systems, and is especially useful reduced-calorie foods.</p>			

**FOR THE PURPOSES OF INFORMATION ONLY**

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AT	Austria	GB	United Kingdom	MR	Mauritania
AU	Australia	GE	Georgia	MW	Malawi
BB	Barbados	GN	Guinea	NE	Niger
BE	Belgium	GR	Greece	NL	Netherlands
BF	Burkina Faso	HU	Hungary	NO	Norway
BG	Bulgaria	IE	Ireland	NZ	New Zealand
BJ	Benin	IT	Italy	PL	Poland
BR	Brazil	JP	Japan	PT	Portugal
BY	Belarus	KE	Kenya	RO	Romania
CA	Canada	KG	Kyrgyzstan	RU	Russian Federation
CF	Central African Republic	KP	Democratic People's Republic of Korea	SD	Sudan
CG	Congo	KR	Republic of Korea	SE	Sweden
CH	Switzerland	KZ	Kazakhstan	SI	Slovenia
CI	Côte d'Ivoire	LI	Liechtenstein	SK	Slovakia
CM	Cameroon	LK	Sri Lanka	SN	Senegal
CN	China	LU	Luxembourg	TD	Chad
CS	Czechoslovakia	LV	Latvia	TG	Togo
CZ	Czech Republic	MC	Monaco	TJ	Tajikistan
DE	Germany	MD	Republic of Moldova	TT	Trinidad and Tobago
DK	Denmark	MG	Madagascar	UA	Ukraine
ES	Spain	ML	Mali	US	United States of America
FI	Finland	MN	Mongolia	UZ	Uzbekistan
FR	France			VN	Viet Nam
GA	Gabon				

5       **"COPROCESSED PARTICULATE BULKING AND FORMULATING AIDS."**

This invention relates to new functional bulking and texturizing materials, their composition, production and use, particularly their use as food ingredients. More particularly, the invention relates to an improved particulate coprocessed cellulose and its manufacture and use.

10      In this era of calorie consciousness in which many consumers are interested in reducing their calorie intake, particularly their fat intake, without reducing their food consumption, there is a need for reduced calorie food ingredients that provide bulk, but few, if any, calories. These bulking aids can be incorporated into specific foods to replace or otherwise reduce the  
15 amount of fat and/or other calorie source that would normally have been present in the food. Typically, although not always, these bulking aids preserve the texture of the food and the mouthfeel of the food and preferably enhance either the functionality of other food ingredients or the efficiency of the process of forming the foods.

20      Cellulose is one such material that has historically served as a functional formulary aid in a wide range of food applications. The use of cellulose as a non-nutritive bulking agent in food systems is limited by several characteristics of cellulose. These include an inherent chalky or other disagreeable taste, especially at high use levels; difficulty in forming a  
25 dispersion which adversely affects its mouth feel; and an adverse effect on texture or consistency.

The traditional approach to overcoming these limitations has been to coat the particulate cellulose with carboxymethyl cellulose, with a gum such as guar gum, or with some other hydrocolloid. Such coatings work with  
30 various degrees of effectiveness in aqueous systems; however, they do not tend to work well in systems containing little or no water.

This invention is directed to a novel particulate cellulose composite that is dispersible in a mid-range or in a high moisture system. The composite can be designed, if desired, to provide good texture and/or to avoid the  
35 chalky taste of cellulose.

The present invention is directed to a composite of a particulate cellulose and one or more surfactant(s) in which the surfactant is adsorbed onto the surface of the cellulose. This composite can be made by coprocessing a particulate cellulose with a surfactant. In addition, the

composite can be used as an ingredient in a food, particularly an mid-range or a high moisture food.

The term "cellulose" denotes a particulate cellulose that has not been coprocessed with a hydrocolloid or with a surfactant. Such a particulate

5 cellulose includes microcrystalline cellulose (MCC), such as Avicel® microcrystalline cellulose, a product of the FMC Corporation; a cellulose powder, such as SolkaFloc® cellulose powder, a product of the Fiber Sales and Development Corporation, a subsidiary of Protein Technologies; a fibrillated cellulose, a fibrillated microcrystalline cellulose, an attrited

10 microcrystalline cellulose, an attrited fibrillated cellulose, and any other particulate cellulose or microcrystalline cellulose. Any cellulose source can be used. These sources include wood pulp, non-woody plant sources such as wheat fiber, soy fiber, cane, bagasse, sugar beet, cocoa, oats, and the like. The starting particle size may range from 1.0 to 500 micrometers

15 (microns;  $\mu$ ), with a preferred range of 1 to 50  $\mu$  for most cellulose, and a most preferred range of from 1 to 20  $\mu$ . The shape of the particles may be round or spherical, rod-like, platelet shaped, or irregular. The preferred particle size and shape are determined by the particular end use, and the general considerations operative in such a selection are known in the art.

20 The term "surfactant" denotes a chemical compound with a calculable HLB (hydrophilic/lipophilic balance) within the range of from 1 to about 40. A surfactant has at least two types of moieties, a hydrophilic moiety and a hydrophobic moiety. Although HLB was developed as a means for categorizing emulsifiers according to their tendency to form emulsions

25 containing oil and water, the HLB system has been and here is applied to surfactants. Generally, the lower the HLB the greater the tendency is for the surfactant to dissolve in oil, and the higher the HLB the greater the tendency is for the surfactant to dissolve in water. A low HLB surfactant has an HLB of about 2 to 8 and is usually oil soluble or at least oil

30 dispersible. A high HLB surfactant has an HLB of about 13 or greater and is usually water soluble or at least water dispersible. Intermediate HLB surfactants have intermediate tendencies. This system, which was developed by Griffin at ICI America, is now a widely accepted empirically derived standard that is used to help select alternative surfactants based on

35 the HLB of the surfactant being used. It is also used to select groups of

- 3 -

surfactants which individually may not have the desired HLB, but collectively have a net HLB within the needed range.

The term "surfactant" as used herein does not include any hydrocolloid. Hydrocolloids are naturally occurring colloidal products, typically gums such 5 as carboxymethyl cellulose(cmc), carrageenan, pectin, agar, konjac, and gelatin, which have hydrophilic moieties, but not hydrophobic moieties. Hydrocolloids are sometimes used as protective colloids or as stabilizers for emulsions and suspensions. Some have also been processed with cellulose. Hydrocolloids are not, however, considered to be surfactants 10 within the context of this invention.

The term "mid-range moisture" denotes a moisture content within the range of greater than 30 weight percent up to but no more than 40 weight percent.

The term "high moisture" denotes a moisture content greater than 40 15 weight percent.

This invention is directed to a novel cellulose composite and to methods for its preparation and use. The novel composite is the product of a cellulose that has been coprocessed with surfactant. This composite is characterized in that its surface properties have been modified to customize 20 its hydrophobic or hydrophilic characteristics, as required by its desired end use properties. Other end use properties that can be controlled include the degree of dispersibility and the potential use levels, especially in the mid-range and high moisture systems of this invention, and the masking of the "chalky" taste sometimes found in cellulosics at high use levels. Generally, 25 the composite has a size within the range of from about 1 to about 505 $\mu$ ; preferably it has a size within the range of from about 1 to about 55 $\mu$ ; and most preferably, it has a size within the range of from about 1 to about 25 $\mu$ .

For the composite of this invention, a surfactant having an HLB within the range of from 1 to 40 can be used, an HLB of >10 is preferred, an HLB 30 of 7-25 is more preferred, and an HLB of 13 to 18 is most preferred. The term HLB in this context includes not only the HLB of a single surfactant, but the effective, net HLB of a combination of surfactants. The HLB of the composite is essentially the same as the HLB of the surfactant or surfactants used to make it. Examples of materials suitable in the broad 35 aspect of this invention may be found in McCutcheon's Emulsifiers and

- 4 -

Detergents (MC Publishing, Glen Rock, N.J.). For the food uses contemplated herein, suitable surfactants are listed in the Food Grade section of McCutcheon's. These include but are not limited to food-grade lecithin, fractionated lecithin, monoglycerides and diglycerides; esters of

5 monoglycerides and diglycerides with acetyl, lauryl, ethoxyl, succinyl, ricinoleic, or diacetyl tartaric groups; polyglycerol esters, propylene glycol esters, sorbitan esters, derived sorbitan esters such as polyoxyethylene sorbitan, and sucrose esters. Fats, oils, proteins, other lipid materials, and blends of the above are also included. For such blends, the term HLB

10 denotes the HLB of the blend, not the HLB of any particular surfactant in the blend. For food use, the surfactants used should be those that are generally recognized as safe for such use by the appropriate regulatory authority. Such recognition may vary with venue.

Some of the food grade surfactants listed in McCutcheon's are

15 provided by their trade name, common name, manufacturer, ionic character, HLB, and use as follows: Alcolec 628G Lecithin/ coconut oil nonionic; Aldo® DC fractionated ester, a product of Lonza Inc., nonionic (HLB 2.0) emulsifiers used in baking, ice creams, and general use in foods; Aldo®MOD FG, glycerol mono/dioleate dispersible nonionic (HLB=4.0);

20 Aldosperse® O-20 FG, 20% Polysorbate 80/ 80% glycerol monostearate, nonionic (HLB=5.0) a frozen desert emulsifier; Capmul GMVS-K glyceryl mono shortening, a product of Capital City Products, nonionic (HLB=3.4), shortenings for cakes and icings, margarine, whipped topping; Caprol 2G4S diglycerol tetrastearate, a product of Capital City Products, nonionic (HLB=2.5); Caprol 3GS Triglycerol monooleate, a product of Capital City Products, nonionic (HLB=6.2) a whipping agent, stabilizer, frozen desserts, fat reduction; Caprol 3GVS Triglycerol mono shortening, a product of Capital City Products nonionic (HLB=6.0) icings, shortenings; Cetodan acetylated monoglycerides, a product of Grinsted Products, nonionic (HLB=

25 1.5) food emulsifier, aerating agent for shortenings, toppings, cakes, edible coating, plasticizer for chewing gum base, antifoam agent, lubricant; Dimodan Distilled monoglycerides, a product of Grinsted Products, nonionic (HLB= 3.8-5.3) food emulsifier for starch complexing, margarine, icings, shortenings, whipped toppings, vegetable, dairy systems, bakery

30 35 hydrates, peanut butter, stabilizer, instant potatoes; Dur-Em®mono and

- 5 -

diglycerides with citric acid, a product of Durkee Industrial Foods, nonionic (HLB=3.3) frozen desserts, caramels, dried potatoes; Famodan® Sorbitan esters of fatty acids, a product of Grinsted Products, nonionic (HLB=2.3-7.7) food emulsifiers for fat crystal modification and bloom retarders;

5 Ice™ No.2 blend of vegetable fat derived mono- and diglycerides with polysorbate 80, a product of Durkee Industrial Foods, nonionic (HLB=5.4) ice cream, milk, melloine, frozen desserts; Panodan Diacetyl tartaric acid esters of monoglycerides, a product of Grinsted Products, anionic (HLB=8.0) food emulsifiers for baked products and mixes to improve

10 structure, volume, dough tolerance, shortenings, low pH emulsions, improve food suspensions, imparts freeze/thaw stability; Span 60, Sorbitan monostearate, a product of ICI Americas, nonionic (HLB=4.7) cake and cake mixes, icings, fillings, confectionary coatings and cocoa products to retain gloss, coffee whiteners, whipped toppings, flavors, antifoam, mineral

15 oil; or wax protective coatings for fruits and vegetables, rehydration aid for dry yeast; Tween 80 POE(20) sorbitan monooleate, a product of ICI Americas, nonionic, (HLB=15) emulsifier for icings and fillings, whipped toppings, shortenings, dietary supplements, flavors, gelatin desserts, poultry defeathering scald water, antifoam, crystallizing aid for salt; Acidan citric

20 acid ester of monoglycerides, a product of Grinsted Products, anionic,(HLB=11.0) for frying margarine and meat emulsions; Aldosperse® MS-20 FG a POE 20 glycerol monostearate, a product of Lonza Inc., nonionic (HLB=13.0) used as a bakery and general food emulsifier; Capmul EMG, an ethoxylated GMS, a product of Capital City Products Co., nonionic

25 (HLB=13.1), used as a dough conditioner for yeast-raised baked goods; Capmul POEL polyoxyethylene (20) sorbitan monolaurate (polysorbate 20), a product of Capital City Products Co., nonionic (HLB= 16.7) used as a solubilizer for flavors; Capmul POE-S polyoxyethylene (20) sorbitan monostearate (polysorbate 60), a product of Capital City Products

30 Co.,nonionic,(HLB=14.9) used in icings, frozen desserts, whipped toppings, and coatings; Clearate WDF soya lecithin, a product of W.A.Cleary Corp, nonionic (HLB=8.0) used in icings, cakes, and instant cocoa.

An effective percentage of surfactant for the composite is about 1% to 50% by weight of the composite. The amount of surfactant required has

35 been found to vary somewhat with surfactant, with 5-10 wt % being required

- 6 -

in some situations, with a lower surfactant percentage being effective in others, and with higher surfactant percentages being better in still other situations. Below 1% of surfactant there is insufficient surfactant to satisfactorily modify the surface properties of the cellulose. As the 5 percentage of surfactant increases, the surface of the composite increasingly tends to approach the properties of the surfactant. The optimum surfactant percentage can be determined without undue experimentation; it changes with the particle size, the surfactant used, and the nature of the system the composite is to be used in are considered. At 10 high surfactant percentages, the properties of the surfactant can begin to dominate or become more dominant, especially if the particle size is large. As the particle size decreases, the amount of surfactant required to provide satisfactory masking of the undesirable inherent properties of the cellulose increases. Thus, a 500 micron particle can be satisfactorily coated with 1% 15 surfactant, whereas a 1 micron particle requires a higher percentage of surfactant to adequately cover the surface. As the particle size increases, adding the same percentage of surfactant as required for the small particle size results in the needless addition of unwanted calories found in the surfactant. Thus the preferred percentage of surfactant is within the range 20 of 1 wt % to 50 wt %, and a more preferred percentage of surfactant is within the range of 3% to 30% of the total; an even more preferred percentage of surfactant is within the range of 3 wt % to 20 wt %; and a most preferred percentage of surfactant is within the range of 5 to 15 wt %.  
Coprocessing is accomplished by any of several physical processes.

25 These include co-processing a mixture of a cellulose with an emulsion, a suspension, or a solution of surfactant. Suitable processes, alone or in combination, include intensive co-milling of cellulose and surfactant, either wet or dry using a bead mill, such as a Dynomill, or a mechanofusion processor; high-intensity mixing using a Henschel, a Littleford-Day or other 30 suitable mixer; spray-drying; bulk co-drying using a fluid bed dryer or some other suitable dryer; fluid bed drying or agglomerating using a Glatt dryer or other suitable dryer; air drying; freeze drying using a Stork dryer or other suitable dryer; or spray chilling of emulsified, or suspended cellulose and surfactant using a Niro or other suitable spray chiller; or by coextrusion of 35 the cellulose and the surfactant, using any one of a number of commercially

available extruders. When wet-processed, the liquid may be water, a non-aqueous solvent such as alcohol, or a mixture thereof. Agents that improve the compatibility of the components may also be used in any of the above processes. A preferred process includes high-intensity mixing in an

5 aqueous solution followed by either co-spray drying, or high-intensity, dry co-milling.

Coprocessing is required. The simple blending of cellulose and surfactant is not sufficient to produce the novel composites of this invention. To form such a composite, the surfactant must be free to flow onto the

10 surface of the cellulose. Such flow can occur near, at, or above the melting temperature of the surfactant or it can occur if the surfactant is in solution or if the surfactant is dispersed or emulsified. A typical process used for making the composites of this invention involves a high shear with a temperature that is sufficient to melt, to soften, or to otherwise improve the

15 flow characteristics of the surfactant. The intensity must be sufficient to force association between the hydrophilic surface of the starting cellulose, and at least the less hydrophobic part of the surfactant molecule, requiring a significant energy input, either mechanically or through a solvent system.

As a general rule, the more uniform the distribution of surfactant is

20 throughout the surfactant/cellulose system being coprocessed, the better the composite. Absent such a distribution, the surfactant will tend to aggregate particles of surfactant rather than coat individual particles. A high degree of surfactant distribution leads to a more effective use of the surfactant on the cellulose and it leads to a more uniform composite particle

25 size distribution. A more uniform composite particle size distribution provides greater quality control in the food or other end product for the composite. Thus, the finer the surfactant dispersion or the greater the degree of emulsion in the coprocessing, the better the product will be.

Coprocessing creates a physical interaction between the cellulose particle

30 and the surfactant; however, it is hypothesized that it generally does not tend to create covalent chemical bonding.

It is critical to the invention that the resulting composite be substantially dried before use. Generally the composite has a maximum moisture content of less than about 10 wt %, preferably less than about wt 6 %, and

35 most preferably in the range of 2-5 wt %. The drying process fixes the

- 8 -

surfactant onto the surface of the cellulose in a manner that tends to prevent, or at least retard, its being stripped from the surface of the cellulose by solvent.

The resulting dry composite is a free-flowing powder that may be added  
5 directly to a final-use system, such as, but not limited to, a food product.  
Since the composite can be added as a dry powder, the mere use of such a  
composite will not appreciably increase the moisture content of the food to  
which it is being added. Thus, the composite can be used in foods having  
extremely low moisture requirements, such as fat phase confections and  
10 cookie fillings.

The composite can, however, be used in a mid-range or in a high  
moisture food, such as a pudding, a bread, a cake, a syrup phase  
confection, a margarine, a salad dressing, a non-dairy creamer, a mellarine,  
or a whipped dessert. Although a few products in this category may have  
15 less than 30 weight percent water, in most cases, these foods have greater  
than 30 weight percent water.

In some of these products, the water is bound and is not available to  
disperse the composite. Available water is a term which describes not the  
absolute amount of water contained in a product, but rather the amount of  
20 water in the product that is not chemically bound.

The composite of this invention is a cellulose, the surface of which has  
been physically modified by a surfactant, with the composite assuming  
some of the surface properties characteristic of the surfactant. For  
example, on the one hand, a cellulose coprocessed with a hydrophilic  
25 surfactant has a lipophobic character; easily dispersing in water without  
settling, but floating in oil without dispersing; on the other hand, a neat  
cellulose clumps, rather than disperses in an oil, while a neat cellulose  
disperses in water with instantaneous settling. This novel surface  
characteristic of the coprocessed material is maintained even after it has  
30 been washed in water. This would not be expected if the composite were  
merely a simple mixture. It is obtained because the composite is not a  
simple mixture, but a cellulose having the surfactant affixed thereto. Thus,  
the composite can be used in systems that have a mid-range moisture  
level, or a high moisture level.

- 9 -

Using the guidelines described herein, a composite can be prepared which effectively masks the objectionable chalky taste and mouthfeel of cellulose, such as microcrystalline cellulose. Thus, a coprocessed cellulose dispersed in a food will not exhibit a chalky mouthfeel even when used in

5 high concentrations. This is true despite the opportunity, during the sometimes extended processing of the food, for the surfactant and the cellulose to become separated by dissolution of the surfactant in the food, or otherwise. In contrast, an unmodified cellulose added to a similar food composition still has the chalky taste and the other properties of neat

10 cellulose.

The composite is used primarily as either a low calorie bulking agent or as a texturizer. In general, any food system may potentially be improved by using the composite to lower its fat and/or its caloric content, or to alter its rheology or its texture. Thus, the composite may be useful in a baked good

15 as a processing agent, because the high HLB of the surfactant permits or improves the kneading of moist dough, while at the same time the composite is compatible with and able to be incorporated into the structure of the finished baked good, where it serves as a bulking agent. The composite may be useful in a margarine having a mid-range or a high

20 moisture content as a processing agent, as a texturizer, or simply as a bulking agent. Alternatively, in a liquid spread, or in a margarine, the composite may serve to stabilize the system, whether the system is an emulsion or a dispersion.

The composite is generally designed to be incorporated into those

25 systems that have an intermediate or a high moisture level. Depending on the particular end use, 1 to 35 weight percent composite can be used in such a food system. One to 20 wt % is preferred, while 1 to 10 wt % is most preferred. The percentage used will be a function of the desired caloric and surface characteristics of the finished food. The usage level will

30 be lower in those instances where the composite is used in conjunction with other bulking agents or the composite is used as a bulking agent in a food that has a low fat content to begin with. The usage level will be higher where the composite is the sole bulking agent.

Industrial and other non-food uses are also contemplated. Potential

35 uses include systems having a mid-range or high moisture content, such

- 10 -

as the following: water based lotions, ointments, cosmetic facial creams. The ability to act as a finely-dispersible source of surfactant can be important in such systems.

Other uses are suggested by the list of surfactants reported in  
5 McCutcheon's, since the composite has many of the characteristics of the surfactant it is made of. Thus, any use accorded the emulsifier is potentially a use for the composite.

Because the ratio of surfactant to cellulose in the composite is variable within broad limits, by tailoring the HLB and composition of the surfactant  
10 portion of the mixture, and by choosing the particle size of the cellulose component, compatibility with particular systems can be optimized for any contemplated end use. This tailoring can be accomplished without undue experimentation simply by choosing surfactants and particle sizes otherwise known to be effective in the particular system. Such procedures are known  
15 in the art. For example, methods of selecting surfactants, and some suggestions for certain food systems, can be found at p. 404 in the "CRC Handbook of Food Additives" (T E Furia, ed.; second edition, volume I; CRC Press, Cleveland; 1972). HLB is described by Rosen ("Surfactants and Interfacial Phenomena," Wiley, NY, 1978; p. 241-49). Flack and Krog  
20 (Lipid Tech. 2 p 11-13, 1990) describe selection of emulsifiers. A list of suitable emulsifiers, and suggestions for their use in particular foods, can be found in industry listings, such as McCutcheon's Emulsifiers and Detergents (MC Publishing, Glen Rock, NJ).

All suitable coprocessing methods result in the formation of a surfactant  
25 layer over at least part of the cellulose particle's surface: This layer, which may be either a continuous or a discontinuous layer, is sufficient to modify the general surface characteristics of the cellulose particle, and is generally hydrophilic, but may in some instances be lipophilic. As a result, the composite bulking agent, consisting of the coprocessed cellulose and  
30 surfactant, is generally compatible with mid-range and high moisture content systems. The coprocessed material is very flexible, in that the HLB of the coprocessed material can be adjusted during its manufacture to have a HLB suitable for a particular use, simply by selecting the HLB or other properties of the surfactant used. The coprocessing step may also be used  
35 to modify or to tailor the composite functionality in food by controlling the

- 11 -

particle size, the particle size distribution, the particle shape, and the ingredients used.

Compared to cellulose alone or to a cellulose and a surfactant added separately to a food system, the coprocessed material improves the taste of 5 the finished food by a reduction or an absence of the well-known dryness or astringency which is inherent in cellulosic materials under low-moisture conditions. This allows the use of cellulose as a bulking agent in materials where it is desirable but was previously not acceptable, and especially allows the use of higher levels of cellulose. Thus, while prior-art cellulose 10 can be objectionable above a few percent, the coprocessed composition of the invention can be used at levels of 10 to 20% when the appropriate surfactant is selected.

In addition, the composite can make a significant improvement in the texture of the food, especially in the mouthfeel and in the melting properties 15 of the food. The composite can also improve the rheology of the food being processed by positively affecting mixing, forming, filling, packaging, or other processing parameters. The composite may also improve the rheology of the finished food. For example in low fat margarine, the use of the composite in a margarine can significantly reduce the viscosity of the 20 margarine despite the addition of higher levels of solids, thereby improving the coating properties of the margarine, without affecting its taste or mouthfeel.

The inventive coprocessed material, if made from an appropriate HLB level surfactant, readily disperses in a mid-range or a high moisture food. 25 In contrast, the unprocessed cellulose alone, and often the surfactant itself, may be poorly dispersible in such systems. The coprocessed material further provides an improvement some food systems, by serving as a processing agent, a texturizer, a stabilizer, a low calorie bulking agent, or by serving as some combination of these functions.

30 The following examples are intended as a further illustration of the invention, but not as a limitation on the scope of the invention. All parts and percentages in the examples, and throughout this specification and claims, are by weight, and all temperatures are in degrees centigrade, unless otherwise indicated.

- 12 -

Example 1

Preparation of a Coprocessed Cellulose Surfactant Ingredient

Avicel® FD 006 microcrystalline cellulose, a product of FMC

5 Corporation, has an average particle size within the range of about 5 to 10 microns. Of this material, 1846.15 g. was dispersed in 11,287.15 g. of deionized water that had been heated to 82.2°-93.3°C (180-200°F). The dispersion was processed using a Gifford-Woods Colloid Mill set at 70% speed (approximately 4900 rpm) and at 40 mil clearance. Then 200 g. of a  
10 surface active agent, a Polycon S60K sorbitan monostearate, a product of Witco Corporation having an HLB about 4.7 was first heated to 76.7°C (170°F), then added to the Avicel dispersion in the colloid mill. The mixture of dispersed Avicel and emulsifier was maintained at a temperature of 71.1°C (160°F) to keep the emulsifier above its melting point and in a liquid  
15 state. The mixture was then homogenized at 60.0°-65.6°C (140-150°F) using a Manton-Gaulin homogenizer set at 17236 kPa (2500 pounds per square inch) (13790 kPa (2000 psi), first stage, 3447 kPa (500 psi) second stage). The homogenized mixture at 60.0°C (140°F) was then pumped by a Moyno pump from a holding tank to the spray head of a two-fluid nozzle  
20 atomizer that was located in a Stork Bowen 91cm (3 foot) diameter spray dryer. The material was atomized at 680 kPa (90 psi) air pressure using a .254 cm (0.1 inch) nozzle, and then dried at 175°C inlet temperature and 90°C outlet temperature. The final material was dried to 2-4% moisture and was screened through a U.S. 60 mesh screen to produce a fine free flowing  
25 powder. This material can be used for a confectionery filling, such as for a caramel, a peanut butter filling or a spread.

Example 2

Coprocessed Ingredient from a Cellulose Floc

30

Eight hundred fifty grams of Solka Floc® 200 FCC cellulose powder, a product of Fiber Sales and Development Corporation, a subsidiary of Protein Technologies, having a mean particle size 35 µ was slurried into 9000 grams of water heated to a temperature of 93.3°C (200°F). One

35 hundred-fifty grams of sorbitan monostearate, a lipophilic surfactant having

- 13 -

a HLB of about 4.7 and a melting point of 54.4°C (130°F), was melted and gradually added to the hot cellulosic slurry circulating through a Gifford Wood colloid mill (10 mil clearance) to produce mechanical emulsification of the surfactant in the continuous water phase. The resulting emulsion was

5 passed through a two stage Manton Gaulin homogenizer first at 17236 kPa (2500 psi) then at 3447 kPa (500 psi), and then spray dried to form a powder.

The spray drying was performed as follows: The homogenized slurry was atomized by feeding it at 680 kPa (90 psi) atomizing air pressure to a  
10 91 cm (3 foot) Bowen spray dryer having a nozzle with a .254 cm (0.1 inch) atomization opening. The slurry was fed to the dryer by means of a variable feed Moyno pump at a rate to provide the desired outlet temperature. The operating inlet and outlet air temperatures of the spray dryer were about 150°C and 80°C, respectively. A free-flowing powder was obtained.

15 Essentially normal cellulose particles were observed when the free flowing spray dried powder was placed on a microslide and examined microscopically. Heat applied directly to the microslide with a hair dryer liquefied the particle surface layer and produced a puddling of material at the bottom of the cellulose particles when the melt point of the lipid layer  
20 was exceeded. The spray dried powder containing 85% cellulose and 15% sorbitan monostearate was reconstituted in water at 10% solids by vigorous hand-stirring. The coprocessed powder tended to float and to collect on the surface of the water. As a control, uncoated (not coprocessed) cellulose powder was added to water; it readily dispersed, swelled and remained  
25 suspended for several minutes.

Example 3  
Dry Coprocessing

30 Mechano Fusion is a technology for coprocessing two or more materials to obtain a modified material in which one of the materials is deposited onto the surface of another. The technology is based on using high intensity mixing and a compaction device. Ninety grams of Avicel® FD006 microcrystalline cellulose, a product of FMC Corporation, and 10  
35 grams of Polycon® 60 sorbitan monostearate, a product of Witco Corp.

- 14 -

having an HLB of about 4.7, were dry blended and placed in the Mechano Fusion® AM-15 coprocessor, a product of Hosokawa Micron International Inc. Shear was generated by the high intensity mixing and compaction and was monitored by an increase in the temperature of the powder. The

5 powder was mixed, compacted, and scraped off of the walls of the chamber and the process was repeated. During the process, the temperature increased because of the intense shear. For this particular sample the process was stopped after the temperature reached 71.1°C (160°F) for 5 minutes, which allowed the surfactant to melt.

10 The resulting dry, coprocessed powder dispersed easily in oil, significantly faster than microcrystalline cellulose alone. When added to water the coprocessed powder floated on the surface; it would wet and settle to the bottom of the flask only after prolonged stirring; however, a non-coprocessed cellulose, such as the Avicel® FD006 microcrystalline

15 cellulose, settled to the bottom immediately. This water washed composite, after prolonged high shear stirring in water and after the water was decanted, was air dried to a constant weight. This dried powder also would not wet easily when added to water indicating that the surface of the coprocessed microcrystalline cellulose was still modified compared to

20 untreated microcrystalline cellulose.

Example 4

Coprocessing in a Non-Aqueous Processing Fluid

25 An alternative method for coating MCC with a surfactant is by dissolving the surfactant in a solvent, adding the dissolved surfactant to MCC, mixing the MCC with the surfactant and evaporating the solvent. Thus, 10 g of Polycon 60® sorbitan monostearate, a product of Witco Corp having an HLB of about 4.7, was dissolved in 100 g of 2-propanol at 60°C. Then 90 g

30 of fine grind MCC was added to the solution and stirred with a laboratory mixer for 5 min. The resulting paste was spread in a 15 cm (6 inch) cake baking dish and dried at 50°C. The resulting powder was evaluated in a manner described in Example 3. The powder performed very similarly to the powder in Example 3.

- 15 -

Example 5  
Use in Peanut Butter.

A sample of coprocessed microcrystalline cellulose composite prepared

5 as in Example 1 was incorporated and tested in a formulation for reduced fat peanut butter as a bulking agent according to the following procedure: To 100 g of a commercial creamy peanut butter was added 10 g of the composite; and, as a control, 10 g of the parent, non coprocessed cellulose was added to a corresponding 100 g sample of the same commercial

10 'creamy' peanut butter. The samples were mixed in a Hobart mixer for 10 minutes at speed #1; then mixed for 30 minutes at speed #2. Between mixing sequences, any wall build-up was returned to the general mixture using a spatula.

The product with the composite had a creamy texture and was

15 smoother than a comparable material made using the parent cellulose. The sample made with cellulose alone was dry and chalky, was slower to melt, and was more viscous after melting, compared to the parent peanut butter or to the peanut butter made with the composite.

20                   Examples 6 (a-o)  
                      Use in Chocolate

Coprocessed compositions and control compositions using cellulose were used in the following procedure for making chocolate. The amounts

25 and proportions of the various non-cellulose ingredients are variable in the art. In the following example of a basic chocolate recipe, cellulose or a coprocessed cellulose/surfactant ingredient is assumed to be added at 10% of the weight of the entire composition. Addition of cellulose-based ingredients at other levels (5%, 13%) was also done; the approximate use

30 levels can be found simply by altering the weight of cellulose added.

1. Mix chocolate liquor (9%), sugar (45%), milk powder (for milk chocolate) (14%), a portion of cocoa butter (about 15%, of a final total of about 22%), and coprocessed material or control cellulose (at 10% when present), in a Sigma/Z mixer for 10 to 20 minutes with a jacket temperature

35 set at 54.4°C (130 °F). (Dry ingredients are preblended prior to mixing.)

- 16 -

Adjust the consistency of the final dough mass with either added cocoa butter or a longer mixing time.

2. Refine the dough mass immediately on a Day 5" x 12", 3- roll refiner. Adjust the feeder rolls to deliver consistent mass to refining rolls; adjust the refining rolls to reduce the particle size to a uniform minimum of 20 microns. For milk chocolate, cooling water at 14.4°C (58°F) may be needed to maintain a finished refined mix temperature of under 60.0°C (140°F); dark chocolate can be processed at a higher temperature.
3. & 4. Conching 1 and 2: Conch in either of two continuous processors set in series for a continuous process; or conch for 8-12 hour in a Sigma mixer for a batch process. First, set to dry conch; second set to wet conch: add cocoa butter (the rest of the 7% saved from the first step) and lecithin (0.5%) if required to reduce process viscosity in the finish conch. Product temperature during the process should not exceed 87.8°C (190°F) for dark chocolate, or 65.6°C (150°F) for milk chocolate.
5. Temper the finished chocolate as follows: Pour out about 2/3 of the warm finished chocolate onto a marble table. Spread the chocolate into a thin layer about 64 cm (1/4 inch) deep onto the table. Work the chocolate by scraping and respreading until the mass is cooled to 30.0°C (86°F) for dark chocolate and 27.8°C (82°F) for milk chocolate. This will form stable seed crystals of cocoa butter. Reintroduce this cooled mass back into the container and mix vigorously with the rest of the chocolate. The final temperature should reach 33.3°C (92°F) for dark chocolate and 30.0° (86°F) for milk chocolate in order for the entire mass to now crystallize into the most stable crystal form for cocoa butter.
6. Pour the tempered chocolate into moulds and tap to even the mass and remove excess air. Cool quickly with good ventilation at 18.3°C (65°F). Cooling will take about 40 minutes. Gently twist and remove the cooled chocolate from the moulds once the chocolate has fully contracted; the store the chocolate at 21.1°C (70°F) to develop optimum gloss and maintain proper temper.

The finished chocolate product produced with a coprocessed cellulose/surfactant material showed several improvements over a chocolate product with cellulose alone. In some variables, it was also an improvement over conventional chocolate. Among these improvements is a

- 17 -

lower process viscosity and yield value, which can be dramatic at 10% and above of the coprocessed material, which is superior to control material containing cellulose alone. These improvements make it much easier to coat confectionery to a defined thickness and uniformity with chocolate

5 containing the inventive composition. In addition, with the coprocessed material, in contrast to cellulose, a higher level of non-nutritive material can be incorporated without adverse taste effects, which leads to a greater reduction of fat and total calories for the finished food.

Also, the coprocessed material demonstrated a great stability in use. In  
10 the extended processing required to make chocolate, there was ample opportunity for the surfactant to become detached from the surface of the cellulose. It is evident from the results of the testing shown below that at least an effective layer of surfactant remained on the cellulose, so that it did not become aggregated and did not revert to the taste of unmodified  
15 cellulose.

#### Sensory Evaluation of Milk Chocolates

Samples of milk chocolate made by the above method with  
20 coprocessed compositions and with cellulose were evaluated qualitatively for taste and texture. Coprocessing was by the method of Example 1, using the Avicel® FD006 microcrystalline cellulose of Example 1, or a related material Avicel® FD008 microcrystalline cellulose, having a significantly larger median particle size (8 µ) than FD006 (about 6 µ). Particle sizes  
25 were measured on a Horiba 7000 particle analyser. The results are reported in Table 1.

In Table 1, "#" denotes an example number, "ratio" denotes the weight percent surfactant in the coprocessed composition, and "% in Choc" denotes the amount of cellulose or coprocessed material added as in step  
30 1. Evaluation was by an expert informal sensory evaluation panel.

- 18 -

Table 1.  
Effect of additives in chocolate.

#	Cellulose Surfactant	Ratio	% in Choc.	Evaluation
5	6a (milk chocolate control, no additives) reference)		none	(standard of
	6b FD006 (none)		10%	less taste, slow
10	6c FD006 (none)		5%	melt, slightly chalky difference less, but
	6d FD006 sorbitan monostearate	20%	6%	still detectable no chalkiness,
15	6e FD006 sorbitan monostearate	20%	10%	like standard no chalkiness; a little
	6f. FD006 sorbitan monostearate	10%	10%	greasy standard - no
	6g FD006 sorbitan monostearate	6%	6%	detectable difference slow melting, palate
20	6h FD006 sorbitan monostearate	6%	4%	adhesion almost standard
	6i FD006 soy lecithin	20%	6%	oxidized lecithin taste; not chalky
	6j FD006 sodium stearoyl lactylate	20%	6%	detergent off- taste, not chalky
25	6k FD006 glycerine	10%	6%	off flavor, waxy texture
	6l. FD006 polydextrose	20%	6%	poor texture, off flavor
	6m FD006 maltodextrin		10%	very chalky, gritty
	6n FD100 (none)		4%	very chalky, dry

30

These tests show that:

35 1. With a preferred surfactant for a particular food, in this case sorbitan monostearate for milk chocolate, very high levels (at least 10%) of a coprocessed cellulose/surfactant ingredient can be incorporated with no effect on texture or taste.

- 19 -

2. With other surfactants differing in HLB, poor taste can result, even if chalkiness is masked. The most successful surfactant employed in this Example 6, sorbitan monostearate, had a HLB of about 4.7. Emulsilac SK, sodium stearoyl lactate, a Witco product that has an HLB of 20 was used,

5 and it appeared to work better as moisture levels increase. Lecithin with an HLB of about 5 and mono,di-glycerides with an HLB of about 2.8 gave taste notes intrinsic to their compositions. Surfactant intrinsic taste is also a variable commonly considered in food manufacture.

3. Coprocessing with materials not of the invention, as in samples 6k,

10 6l and 6m, failed to mask the chalky taste of the cellulose and/or imparted a bad texture, even at low use levels.

Example 7

Preparation of Samples for Quantitative Evaluation of Sensory Effects

15

A standard simple test system was used and prepared by the following recipe. In a 600 ml. beaker, 250 grams. of a hard fat, cocoa butter, was melted by heating on a heating mantle. With constant mixing, using a Caframo mixer set at 500-1000 rpm speed, a quantity of 12.5 grams., 25.0

20 grams., or 50 grams., of the coprocessed ingredient was added and dispersed in the melted fat by stirring. The fat was at a temperature of 48.8°C-60.0°C (120°F - 140°F), which is above the melting point of cocoa butter.

The melted fat containing the dispersed material was poured into forms

25 of about 2.54 cm (1 inch) square (small polyethylene weighting boats). The samples were then set in a freezer for 30 minutes to 1 hour to 'set' the dispersed material in the fat. These samples with varying levels of ingredients were tasted by a specific sensory protocol to characterize and quantify differences.

30

Example 8

Quantitative Sensory Results.

A formal sensory protocol was used to quantify taste and texture

35 differences, using standard sensory panel testing methods. This sensory

- 20 -

protocol identified three groups of attributes affecting the mouthfeel, which were important in understanding the effect of incorporating cellulosic materials in a non-aqueous/low moisture system. These attribute groups were astringency-related, described as drying, roughing, puckering;

5 particle-related, described by overall amount of particles, size, chalkiness; and melt-related, described by melt rate, melt consistency (homogeneity), and by residual mouth-coating.

The results of the testing showed improved mouth feel characteristics in

10 all three attribute groups. Cellulose alone had a considerable gritty or chalky feel depending on the particle size. The coprocessed cellulose/surfactant material significantly reduced those effects. There was also an improvement (decrease) of the "drying, roughing, puckering" effect especially at the higher use levels of the coprocessed material in the cocoa

15 butter medium. Finally, there was an improvement in melt consistency by using a coprocessed material. All these improvements together gave a much more palatable texture.

The averaged results obtained by nine taste testers on the variable "chalky" were obtained, using materials prepared as in Example 7. The

20 coprocessed ingredients were prepared as in Example 1, using Avicel® FD006 microcrystalline cellulose ("cellulose"), a product of FMC Corporation coprocessed with 10% of sorbitan monostearate (sample "S"). Results are shown in Table 2. The numbers obtained are the perceived "chalkiness"; higher numbers indicate a more chalky mouthfeel. Note that the perceived

25 values of the control (no additive) material vary between tests over a range of 0.7 units.

- 21 -

Table 2  
Relative Chalkiness

<u>Additive type:</u>	<u>Cellulose only</u>	<u>Coprocessed "S"</u>
5		
	<u>additive use level:</u>	
	no-additive control	2.4
	5%	2.9
	10%	4.8
10	20%	7.2
		1.7
		2.1
		2.7
15		
20		

At 5% addition, the unprocessed cellulose was not significantly chalkier than the base cocoa butter; however, at 10% and 20% addition, the cellulose-only samples were very significantly chalky. The coprocessed material was similar to the no-cellulose control at a low level of addition; at higher levels, however, the coprocessed material increased in chalkiness only slowly with use level, whereas the cellulose-only control increased rapidly in chalkiness with increasing use level; and even at a use level of 20% the coprocessed sample was not significantly higher than the control level, while the cellulose-only sample was significantly chalkier.

Example 9  
Dispersion of Surfactant

25 A coprocessed material was prepared as in Example 1 with the exception that a small amount of the oil-soluble dye Oil Red O was used with the surfactant. As a control, the surfactant, sorbitan monostearate, was melted, mixed with an equivalent amount of dye, cooled, and cut up into pieces. When added to a room temperature liquid soybean oil, the 30 coprocessed cellulose-surfactant ingredient easily dispersed, producing a smooth viscous suspension, and the dye was extracted from the particles into the oil. When pieces of dyed sorbitan monostearate were dispersed into room temperature oil, the pieces immediately settled to the bottom of the container without dissolution of the surfactant, and the dye was not 35 significantly extracted from the particles. When the solution was heated,

- 22 -

the particles dissolved and the dye was extracted. This demonstrates that the coprocessed material of the invention can also act as a method of dispersing surfactants into a food or other system.

5

Example 10  
Fat Phase Truffle

The following is one method for preparing a fat phase truffle. Dark chocolate is heated in a microwave set at full power for 5 minutes to heat it  
10 to a temperature of 54°C, then placed in a bowl and cooled to 32°C. Nut paste, melted vegetable fat, and flavoring are then added, and the mixture is mixed using a Hobart paddle mixer, first at about speed 1. The mixer speed is then increased to speed 2, with either the composite or the microcrystalline cellulose being added with mixing.

15 The admixture is poured into and spread in a shallow pan; then it is cooled to 30°C or lower, until it is sufficiently firm to scoop with a cookie dropper or a melon scooper; after which it is rolled and dusted with a cocoa powder, using dutched cocoa powder, which contains 10-12% fat.

20 The truffle containing the composite tastes the same as the truffle that contains no cellulose ingredient, and has a better taste and texture than cellulose alone; in this example the use of either the neat cellulose or the composite results in a product having an approximately 10% reduction in fat in the formula, as compared to the control.

25

Table 3  
Fat Phase Truffle

Ingredients	Control %/ grams	Neat Cellulose %/ grams	Composite %/ grams
Dark Chocolate	62.18% 1200 grams	56.99% 1100 grams	56.99% 1100 grams
Hazelnut Paste	31.09% 600 grams	31.09% 600 grams	31.09% 600 grams

- 23 -

Hydrogenated	6.22 %	1.45%	1.45%
Coconut Oil	120 grams	28 grams	28 grams
Rum Flavor	0.52%	0.52%	0.52%
	10 grams	10 grams	10 grams
Composite	0%	0%	9.95%
	0.00 grams	0.00 grams	192 grams
Neat Cellulose	%	9.95%	0%
	0.00 grams	192 grams	0.00 grams
Total	100.00%	100.00%	100.00%
	1930 grams	1930 grams	1930 grams

Preferred ingredients:

Dark chocolate couverture

Pure hazelnut paste

5 Partially hydrogenated palm kernel/coconut, Pureco 90/92, a product of Karlsamns Co.

Natural and artificial Jamaican rum extract FA 34, a product of Virginia Dare.

Avicel®microcrystalline cellulose, Avicel is a trademark of the FMC

10 Corporation.

Composite: 90% Avicel®microcrystalline cellulose/ 10% sorbitan monostearate.

Example 11

15 Caramel

Caramel is a syrup phase confection having a sugar syrup base of water soluble components. Into this base other materials are dispersed to form taste and texture. These components include sweetened condensed

20 milk and butter oil. The milk solids, specifically the proteins in the milk solids, react with the reducing sugars to produce the Maillard reaction known as 'caramelization.' That reaction provides the characteristic color and flavor of caramel. The butter oil provides lubricity to the confections.

In a caramel, the composite functions as a texturizer, which permits the  
25 production of a higher moisture formula, thus giving the manufacturer an

- 24 -

opportunity to reduce the cost of the caramel. The higher moisture also permits a process time reduction because not as much water has to be boiled off to get the proper structure for the soft caramel. Typically each caramel has the same ingredients but different degrees of softness,

5 sometimes called chewiness, which is controlled by the modification of the moisture content. Typically, softness varies with moisture content over a range of from 6 to 12 % moisture based on the weight of the caramel, with very noticeable changes in the texture and flow characteristics of the caramel as it increases in overall moisture content at 2% increments.

10 The use of the composite provides a higher moisture caramel with the same texture and flow characteristics as a lower moisture caramel; thus, a caramel can be made that will have similar texture and flow properties as a caramel that has an approximately 2 % lower overall moisture content. For example, this product permits the production of a caramel with 14%

15 moisture, that will have the same texture and flow as a traditional caramel having 12 % moisture. The composite permits control of graining and cold flow. The texture of the caramel made with the composite has approximately 2% more moisture and 33% less fat than does the control, and is as good as the control. The composite also provides better tooth release and eating

20 quality .

The caramel is prepared by first dissolving salt and then dissolving sugar in water. The solution is brought to a boil at 110°C. While maintaining this temperature, the following ingredients are added with stirring: corn syrup, followed by lecithin, sweet condensed skim milk, butter

25 oil, and then a slurry of composite dispersed in 200 grams of water. The resultant mixture is cooked to 110°C, and is then caramelized at 118°C with a controlled cook time of about 21 minutes. Then 200 grams of water is added and the mixture is quickly brought to a reboil at 118°C for 12 minutes, except that for the caramel containing 10% composite reboil

30 occurs at 114°C. Vanilla is then added with stirring, followed by cooling the mixture to 90°C. This mixture is then transferred onto a slightly greased sheet tray, cooled to room temperature, and cut to any desired shape.

35 The caramel containing the composite is comparable in taste and texture to the caramel without the composite, and has a better texture than caramel with cellulose alone.

- 25 -

Table 4  
Caramel

Ingredients	Control %/grams	Composite %/grams	Composite %/grams
Sugar	20.21% (680g)	18.94% (680g)	18.94% (680g)
Water	13.44% (452g)	18.89% (678g)	18.89% (678g)
63 DE Corn Syrup	33.65% (1132g)	31.53% (1132g)	31.53% (1132g)
Sweetened Condensed Skim Milk	20.21% (680g)	18.94% (680g)	18.94% (680g)
Butter Oil	11.77% (396g)	6.69% (240g)	6.69% (240g)
Vanilla	0.30% (10g)	0.28% (10g)	0.28% (10g)
Lecithin DA 51	0.21% (7g)	0.19% (7g)	0.19% (7g)
Salt	0.21% (7g)	0.19% (7g)	0.17% (7g)
Composite	0% (0g)	0% (0g)	4.35% (156.0g)
Neat Cellulose	0% 0.00 g	4.35% 156.0 g	0% 0.00 g
Total	100% (3364g)	100% (3590g)	100% (3590g)

**Preferred ingredients:**

Dixie Crystals extra fine granular sugar, Savannah Sugar Refinery,  
 5 Savannah Foods and Industries, Inc.  
     Staley Sweetose 4300, 63DE corn syrup, A.E. Staley Manufacturing,  
     Co.  
     Sweetened condensed skim milk, Galloway Co.  
     Anhydrous milk fat, Mid-America Farms  
 10 Two-fold vanilla extract, Virginia Dare

- 26 -

Metarin DA51 lecithin, a product of Lucas Meyer, Inc.

Premier fine flake salt, Cargill Salt Division

Avicel® FD 006 microcrystalline cellulose. Avicel is a trademark of the FMC Corporation.

5 Atmos®150 K glycerol monostearate having an HLB of 3.5. Atmos is a trademark of Witco Corporation.

Composite is a particle with a median size of approximately 10 micron that is an 90/10 w/w Avicel® FD008 microcrystalline cellulose/Atmos®150K glycerol monostearate.

10

Example 12

Fudge

Fudge, like caramel, is a syrup phase confection; however, unlike 15 caramel, fudge includes sugar crystals to shorten its texture; as a consequence, fudge is sometime referred to as a grained confection.

The fudge is prepared by first dissolving salt and then dissolving sugar in water. The solution is brought to a boil at 110°C. While maintaining this temperature, the following ingredients are added: corn syrup, lecithin, sweet 20 condensed skim milk, and butter oil; then followed by a slurry of the composite, which slurry had been prepared by dispersing the composite in 200 grams of water. The resultant mixture is first cooked to 110°C, and then caramelized at 115°C. Then 200 grams of water is added and the mixture is quickly brought to a reboil at 118°C for 12 minutes, except that for 25 the 10% composite containing fudge, reboil occurs in 7 minutes at 114°C. Vanilla is then added with stirring, followed by cooling the mixture to 90°C. Add icing sugar predispersed in sorbitol to set the sugar crystals to grain. This mixture is then poured onto a slightly greased sheet tray, cooled to room temperature, and cut to any desired shape.

30 The recipe used for the control and two different products, one containing a composite, the other containing a neat cellulose, are described in Table 5. The fudge containing the composite has approximately 2% higher moisture and significantly (67%) less fat than the control; yet, the fudge containing the composite is comparable in taste and texture to the 35 control and has a better texture than does the sample with cellulose alone.

- 27 -

Table 5  
Fudge

Ingredients	Control	Neat Cellulose %/grams	Composite %/grams
Sugar	25.04% (1132g)	18.54% (1132g)	18.54% (1132g)
Water	17.52% (792g)	38.92% (2376g)	38.92% (2376g)
63 DE Corn Syrup	25.04% (1132g)	18.54% (1132g)	18.54% (1132g)
Sweetened Condensed Skim Milk	15.04% (680g)	11.14% (680g)	11.14% (680g)
Butter Oil	11.77% (532g)	1.96% (119.6g)	1.96% (119.6g)
Icing Sugar/Fondant	2.50% (113.2g)	1.85% (113.2g)	1.85% (113.2g)
Sorbitol	2.50% (113.2g)	1.85% (113.2g)	1.85% (113.2g)
Vanilla	0.22% (10g)	0.16% (10g)	0.16% (10g)
Lecithin DA51	0.19% (8.5g)	0.14% (8.5g)	0.14% (8.5g)
Salt	0.19% (8.5g)	0.14% (8.5g)	0.14% (8.5g)
Composite	0% (0g)	0.00% (0g)	6.75% (412.4g)
Neat Cellulose	0% (0.00 g)	6.75% (412.4 g)	0% (0.00 g)
Total	100% (4521.4g)	100% (6105.4g)	100% (6105.4g)

- 28 -

Preferred ingredients:

Dixie Crystals extra fine granular sugar, Savannah Sugar Refiner,  
Savannah Foods and Industries, Inc.

Staley Sweetose 4300, 63DE corn syrup, A.E. Staley Manufacturing  
5 Co.  
Sweetened condensed skim milk  
12X fondant and icing sugar  
Neosorb liquid sorbitol, 70/02, Roquette Corp.  
Anhydrous milk fat  
10 Two-fold vanilla extract, Virginia Dare  
Metarin DA51 lecithin, a product of Lucas Meyer, Inc.  
Premier fine flake salt  
Avicel® FDO08 microcrystalline cellulose, Avicel is a trademark of the  
FMC Corporation  
15 Atmos®150K glycerol monostearate having an HLB of 3.5. Atmos is a  
trademark of Witco Corporation.  
Composite is a particle with a median size of approximately 10 micron  
that is an 90/10 w/w Avicel® FD008 microcrystalline cellulose/Atmos®150K  
glycerol monostearate.  
20

Example 13

Nougat

Use the following procedure and the recipe provided in Table 6 to make  
25 a nougat. First predisperse the microcrystalline cellulose control or the  
composite in enough water to make a slurry or a paste. Dissolve sugar in  
water; add corn syrup and malt and cook to 126°C. Add the predispersed  
microcrystalline cellulose control or the composite at this time. Dissolve egg  
albumen in water and invert sugar and whip in a Hobart mixer with a wire  
30 whip, starting with the slowest speed but progressing to the highest speed  
for the final whip. Then add cooked syrup and whip to a density of 0.4-0.5,  
again mixing at the highest speed. Then add cocoa powder and icing  
sugar; follow this with fat addition with slow mixing. The fat must be melted  
to a liquid before this addition; then transfer the final mixture onto a slightly  
35 greased waxed or poly coated paper; cover overnight; then cool, cut to

- 29 -

shape, and enrobe in chocolate. The two samples are similar in taste and in texture to the control.

Table 6  
Nougat

5

Ingredients	Control %/ grams	Neat Cellulose %/ grams	Composite %/ grams
Sugar	27.43% 1300 grams	25.29% 1300 grams	25.29% 1300 grams
Water	8.44% 400 grams	15.56% 800 grams	15.56% 800 grams
63 DE Corn Syrup	33.76% 1600 grams	31.13% 1600 grams	31.13% 1600 grams
Malt Extract	0.84% 40 grams	0.78% 40 grams	0.78% 40 grams
Egg Albumen	0.84% 40 grams	0.78% 40 grams	0.78 % 40 grams
Water	6.33% 300 grams	5.84% 300 grams	5.84% 300 grams
Invert Sugar	10.55% 500 grams	9.73% 500 grams	9.73% 500 grams
Cocoa Powder	2.11% 100 grams	1.95% 100 grams	1.95% 100 grams
Icing Sugar/Fondant	2.11% 100 grams	0.97% 50 grams	0.97% 50 grams
	7.59% 360 grams	4.4% 226 grams	4.4% 226 grams
Cellulose or Composite	0% 0.00 grams	0% 0.00 grams	3.58% 184.0 grams
Neat Cellulose	0% 0.00 grams	3.58% 184.0 grams	0% 0.00 grams
Total	100.00% 4740 grams	100.00% 5140 grams	100.00% 5140 grams

Preferred ingredients:

Extra fine granular sugar

- 30 -

Staley Sweetose 4300, 63DE corn syrup, a product of A.E. Staley Manufacturing Company

Malt Extract # 102 medium, a product of Malt Products Corporation

Egg white solids, spray dried, P-110, a product of Henningsen Foods, Inc.

5 Nulomoline invert syrup, Ingredient Technology Corporation

Dutched 10-12% fat cocoa powder, PD 205, a product of Cocoa Barry

12X fondant and icing sugar, a product of American crystal Sugar Company

Partially hydrogenated palm kernel/coconut oil, Pureco 90/92, a product of Karlshamns Co.

10 Avicel® FDO08 microcrystalline cellulose. Avicel is a trademark of the FMC Corporation.

Triodan55 polyglycerol ester, a product of Grinsted Products, having an HLB of 6.8.

15 Composite is a particle with a median size of approximately 8 to 12 micron that is an 90/10 w/w Avicel® FD008 microcrystalline cellulose/Triodan 55 polyglycerol ester.

Example 14

Chocolate Chip

20

A typical chocolate chip is about 30% fat. The chocolate chip is a dark chocolate that has been prepared as in Example 6, with the exception that it is deposited as a drop. The sensory result good for each of the respective chocolates.

25

Example 15

Pudding

A pudding is prepared, as follows.

30 First a composite is prepared, as follows: A coprocessed fine particle size microcrystalline cellulose (mcc) having a 6 to 8 micron median particle size, is coprocessed at a 80 to 20 weight ratio with a Emulsilac®SK sodium stearoyl lactylate (ssl) (a product of Witco, having an HLB 20) and dried to a fine powder according the the procedure of Example 1.

- 31 -

The pudding is prepared using the ingredients as specified in Table 7, by first mixing the dry ingredients; then adding the ingredient mixture to cold milk; followed by blending the milk with those ingredients.

The mixture is stirred and cooked in a double boiler until thickened at about 82.2°C (180°F), at which time the heat is reduced to a medium setting and cooked with continual stirring for about 15 minutes.

The resulting mixture is cooled slightly within the range of about 48.9°C to 60.0°C (120°F to 140°F); vanilla is then added; and the resulting mixture is poured into molds which are placed in a refrigerator and cooled for 1 or 2 hours.

The Blanc Mange made with the composite is as tasty as that made without composite.

Table 7  
Pudding

Ingredients	Control Weight %	Composite Weight %
1% Fat Milk	84.86	84.86
Sugar	10.37	9.37
Corn Starch	4.53	4.53
80%mcc/20%ssi	0.00	1.00
Table Salt	0.13	0.13
Two-fold Vanilla Extract	0.11	0.11
Total	100.00 %	100.00 %

### **Preferred Ingredients:**

Emulsilac® sodium stearoyl lactylate, a product of Witco Corporation,  
20 having an HLB of 20.

A microcrystalline cellulose having a median particle size of 6 to 8 microns.

Composite is a particle with a median size of 10 to 15 microns that is an 80/20 w/w microcrystalline cellulose/Emulsilac® sodium stearoyl lactylate.

Example 16  
Use in a Bread

5

A bread dough is made by mixing 29 kgs (63 pounds) of a wheat flour, .68 kgs (1.5 pounds) of table salt, .68 (1.5 pounds) of yeast, 16 kgs (36 pounds) of water, and .45 kgs (1 pound) of a lard. The mixture is allowed to sit for 4 hours, and then baked in an oven at 176.7°C (350°F) for one hour.

10

A second bread dough is made by mixing 25.9 kgs (57.2 pounds) of wheat flour, .68 kgs (1.5 pounds) of table salt, 2.86 kgs (6.3 pounds) of composite prepared as in Example 2 (with the exception that Myverol SMG 15 succinylated monoglycerides, a product of Eastman Chemical Products, Inc. having an HLB of 4 to 6, was used as the surfactant), .68 kgs (1.5 pounds) of yeast, 16 kgs (36 pounds) of water, .23 kgs (0.5 pounds) of lard. This mixture is allowed to sit for 4 hours, and is then baked in an oven at 350°F for one hour.

20

One hour after the breads have been removed from the oven, they are compared. The taste and texture are comparable..

Example 17  
Low Fat Meat

25

A low fat meat can be prepared using the following procedure, and the ingredients specified in Table 8. First, trim pork and beef then blend to make a 50:50 mixture at desired fat levels. Chop a lean meat portion, add salt, sodium nitrite and half the volume of water as 50% water/50% ice; then 30 add the remaining dry ingredients; then add what remains of the water and the fat meat blend. Run this mixture through an emulsifier with a 0.4 mm plate; stuff the mixture into casings; cook it in a smokehouse using gradient heating with fast air circulation; then shower it; chill it; peel it; and vacuum package the final product.

- 33 -

For evaluation, the products are simmered in water and served warm without condiments. A sensory preference panel can then evaluate the products, for preference evaluation using a 9-point hedonic scale on which a score of "9" represents an excellent product and a score of "1" represents an extremely poor product.

Using this evaluation process, both the control and the composite containing sample obtain a score of 6 to 7

Table 8  
Low Fat Meat

Ingredients	Control	Composite
	%	%
Lean Meat Blend	20.33	33.92
3.6% Fat		
Composite	0.00	1.50
Fat Meat Blend	52.47	24.38
48.1% Fat		
Water	21.73	34.43
Salt	2.20	2.20
Seasoning	3.22	3.22
Sodium	0.04	0.04
Erythorbate		
Sodium Nitrite	0.01	0.01
Carageenan	0.00	0.30
Total	100.00%	100.00%

#### **Ingredients:**

Gelcarin® XP8004 carageenan. Gelcarin is a trademark of FMC Corporation.

15      Composite is a particle with a median size of approximately 15 to 20 micron that is an 80/20 w/w Avicel® FD008 microcrystalline cellulose/Atmul® 84K mono and diglycerides. Avicel is a trademark of FMC Corporation. Atmul® 84K is a surfactant manufactured by Witco Corporation having an HLB of 2.8.

- 34 -

EXAMPLE 18  
Reduced Fat Chocolate Mousse

A reduced fat chocolate mousse can be made using the ingredients

5    specified in Table 9, as follows. In a first container, dry blend sugar, non-fat milk, milk chocolate crumb, cacao, milk protein, modified starch, gelatin, emulsifier and carrageenan. In a separate container disperse a cellulose/surfactant composite in water with a high speed mixer, preferably of the Silverson type, with about 10 minutes of mixing; then add the dry

10    blend from the first container with continuous stirring. While stirring, bring the heat up to 80°C using a steam-jacketed kettle. Homogenize the mixture at 180 kg/cm<sup>2</sup> to insure proper mixing; then cool to 15°C. Once cooled to 15°, aerate and then deposit into containers.

The chocolate mousse made using the composite is at least as good as

15    the chocolate mousse made using neat cellulose.

Table 9  
Reduced Fat Chocolate Mousse

Ingredients	Cellulose-no composite	Composite
	Percent by Weight	Percent by Weight
Water	64.89	64.45
Sugar	15.00	15.00
Non-Fat Dry Milk	6.10	6.10
Milk Chocolate Crumb	5.00	5.00
Cocoa	2.55	2.55
Milk Protein	2.00	2.00
Modified Starch	2.00	2.00
Gelatin (200 Bloom)	1.75	1.75
Avicel® CL 611 Cellulose	0.50	0.50
Composite	0.00	0.55
Emulsifer	0.11	0.00
Carrageenan	0.10	0.10
Total	100.00%	100%

20    Preferred ingredients:

- 35 -

Lactodan p22k lactic acid ester of monoglycerides, a product of Grinsted Products, Inc. used as the emulsifier in the no composite example and used to make the composite used in the other example.

Avicel®CL611 microcrystalline cellulose. Avicel is a trademark of FMC  
5 Corporation.

A microcrystalline cellulose having a particle size of 10 microns. Composite is a particle with a median size of approximately 15-20 micron that is a 80/20 w/w microcrystalline cellulose/Lactodan p22k

Example 19  
Whipped Topping

A reduced fat, baker's whipped topping can be prepared as follows using the ingredients provided in Table 10.

15        1. Using a high speed mixer, disperse Novagel®RCN 15  
microcrystalline cellulose, in water. Novagel is a trademark of FMC  
Corporation.

20        2. Gradually add a cellulose gum and continue mixing for 5 minutes.  
3. Blend nonfat dry milk and sugar. Add the blend to the above  
mixture and continue mixing for 5 minutes.

25        4. Add corn syrup and start heating to 62.8°C (145°F).  
5. In a separate container, heat the fat and emulsifiers to 60.0°C  
(140°F).

30        6. Add the oil and emulsifiers 60.0°C (140°F) to the aqueous phase  
(batch) when the aqueous phase reaches 62.8°C (145°F) with continued  
mixing.

35        7. Pasteurize the mix at 71.1°C (160°F) for 30 minutes.  
8. Homogenize the mix at 17236 kPa (2500 pounds per square inch)  
9. Cool the mix to 4.4°C (40°F) and age for 24 hours.

40        10. Whipping instructions: Measure 700 grams of the just prepared  
mix into a chilled 5 quart Hobart® mixer bowl. Using a wire whip  
attachment at high speed (#3), whip for 2 1/2 to 3 minutes.

The whipped topping containing the composite is as tasty and as light and as airy as the whipped topping containing cellulose, but no composite

- 36 -

Table 10  
Whipped Topping

Ingredients	Cellulose(no composite) Percent by Weight	Composite Percent by Weight
Water	62.90	61.10
Non-fat dry milk	12.50	12.50
Sugar	9.00	9.00
Partially hydrogenated vegetable oil	7.00	7.00
Corn Syrup, 42 D.E.	6.00	6.00
Novagel ®RCN 15 coprocessed microcrystalline cellulose/guar	2.00	2.00
Composite	0.00	2.25
Polysorbate 60	0.30	0.00
Cellulose gum	0.15	0.15
Distilled monoglycerides	0.15	0.00
Total	100.00%	100.00%

Preferred Ingredients:

5 A Paramount B partially hydrogenated vegetable oil, a product of Van Den Bergh Foods  
 CMC - 7HF cellulose gum, a product of Hercules Inc.  
 Composite is a particle with a median size of approximately 15 to 20 micron that is an 80/14/6 w/w Avicel FD008 microcrystalline cellulose, a

10 product of FMC corporation, and a surfactant that is a mixture of Tween 60, polysorbate 60, a product of ICI Americas, Inc., having an HLB of 14.9 and Myverol 18-06, distilled monoglycerides, a product of Eastman Chemical, having an HLB of 3.8.

- 37 -

Example 20  
Salad Dressing

A reduced calorie heat stable salad dressing can be made as follows,  
5 using the ingredients as specified in Table 11.

Part I

Prepare a cellulose composite as in Example 1 using 80 wt % of a  
microcrystalline cellulose having a median particle size of 8 to 12 microns  
and 20 wt % of Tween®60 a polyoxyethylene sorbitan monostearate, a  
10 product of ICI Americas, Inc., which has an HLB of 14.9.

Part II

Predisperse the cellulose, either the Avicel CL-611 microcrystalline  
cellulose or the composite, in 90 % of the available water using a planetary  
mixer. Then add xanthan gum and hydrate for 10 minutes. To this mixture  
15 add a previously combined Polysorbate 60 and oil in a slow continuous  
stream with mixing for 15 minutes. Add starch slurried in the remaining  
water. Add and blend the remaining dry ingredient, except salt, and mix for  
2 minutes. Add sorbitol solution and mix 2 minutes. Combine vinegar and  
salt and add to the above emulsion, with mixing for 5 minutes. Homogenize  
20 this mixture at 13790 kPa (2000 psi) (1st stage) and 3447 kPa (500 psi)  
(2nd stage) at a total of 17236 kPa (2500 pounds per square inch). Heat in  
a kettle to 71.1°C (160°F) with the main vegetable or meat component. A  
60:40 weight ratio of main component to dressing is recommended. Hot fill  
and retort the total product using good manufacturing process techniques.  
25 The Avicel®CL-611 microcrystalline cellulose and the composite  
samples each performed well, each with about the same results, when  
compared to other dressings.

- 38 -

Table 11  
Salad Dressing

Ingredients	MCC Weight Percent	Composite Weight Percent
Water	54.08	54.08
Vinegar (50 grain)	15.00	15.00
Vegetable oil	12.00	12.00
Sorbitol (70% solution)	10.00	10.00
Avicel® CL-611 MCC	4.50	3.54
Composite	0.00	1.20
Starch-purity 420	2.00	2.00
Salt	1.50	1.50
Mustard Powder	0.30	0.30
Xanthan Gum	0.25	0.25
Polysorbate 60	0.24	0.00
Onion Powder	0.10	0.10
White Pepper	0.02	0.02
Ascorbic Acid	0.01	0.01
Total	100.00 %	100.00 %

5

Example 21  
Non-Dairy Creamer

A reduced fat, non-dairy creamer is prepared using the ingredients specified in Table 12, as follows: Dry blend the ingredients; then mix them with water at 60°C (140°F); then mix in premelted vegetable fat; and then mix in corn syrup. Pasteurize the mixture at 71°C (160°F) for 30 minutes; then homogenize the mixture in a two stage homogenizer having a 17236 kPa (2500 pound per square inch) first stage and a 3447 kPa (500 pound per square inch) second stage. Cool and freeze the homogenized product at -17.8 to -23°C (0 to -10°F).

The non-dairy whiteners are added to coffee, then stirred, and finally tasted. Each appears the same and has the same characteristics for blending and for taste, as does the other.

- 39 -

Table 12  
Non-Dairy Creamer

Ingredients	Control Weight Percent	Composite Weight Percent
Water	74.50%	74.50%
36 DE Corn Syrup	12.75%	12.15%
Solids		
Hydrogenated Soybean Oil	10.0%	10.0%
Sodium Caseinate	2.5%	2.5%
Sodium Stearoyl Lactylate	0.10%	0.00%
Polysorbate 60	0.05%	0.00%
Dipotassium Phosphate	0.10%	0.10%
Composite	0.00%	0.75%
Total	100.00%	100.00%

5 Preferred Ingredients:

Composite is a particle with a median size of approximately 15 to 20 microns that is an 80/14/6 w/w Avicel FD008 microcrystalline cellulose, a product of FMC corporation/Emulsilac®SK sodium stearoyl lactylate, a product of Witco Corporation having an HLB of 20, and Polycon®T60K polyoxyethylene sorbitan monostearate, a product of Witco Corporation having an HLB of 14.9.

Example 22  
Fabricated Frozen French Fry

15

A fabricated frozen french fry was prepared using the ingredients specified in table 13, as follows:

Part I

First a composite is prepared according to the procedure of Example 1 using an initial microcrystalline cellulose having an approximately 10 micron median particle size and Myverol®18-06 a monoglycerides from

- 40 -

hydrogenated vegetable oil produced by Eastman Kodak having an HLB of about 3.8 to provide an 80/20 w/w composite having an median particle size of approximately 25 to 30 median particle size.

Part II

- 5 With a high-speed propeller mixer disperse the cellulose, either the Avicel® cellulose gel or the composite, in the water portion of the batch, mixing for approximately 10 minutes.

Part III

- 10 Completely blend the remaining dry ingredients using a Hobart® type mixer with a wire whip on speed # 1 for 3 minutes.

Place the dry blended ingredients in the Hobart mixer with a paddle type attachment. Set the mixer on # 1 speed, slowly adding the predispersed cellulose prepared in Part I; and then mixing for a maximum of 3 minutes.

- 15 Allow the mixture to stand for 10 minutes to hydrate and develop the dough.

Part IV

Extrude, then cut and pan fry at 173°C (345°F) for 30 seconds, then quick freeze and store.

- 20 To evaluate the product, fry the french fry at 190.6°C (375°F) for 90 seconds; and evaluate under a 60°C (140°F) heat lamp.

Results

- 25 The fabricated frozen french fries made with the composite as well as with those made with the Avicel® microcrystalline cellulose are comparable in quality to those made without either of these two ingredients.

- 30 The composite provides structural firmness and integrity to the dough, thus improving the extrudability of the dough reducing breakage during and after extruding. This structural effect also improves the body and texture of the finished fry providing a smoother consistency, fewer void spaces, and a thinner crust. The result is a more tender but firm fry with a more pleasing mouthfeel.

As the composite level is increased, there is a corresponding increase in the firmness.

- 41 -

Table 13  
Fabricated French Fry

Ingredients	Control Weight Percent	Composite Weight Percent
Potato Granules	26.49	26.49
High Amylose Corn	7.02	5.62
Starch		
Salt	0.70	0.70
Guar Gum	0.53	0.53
Emulsifier	0.35	0.00
Avicel® RC-591F	1.0	0.40
Cellulose Gel		
Composite	0.00	1.75
Water	63.91	64.51
Total	100.00%	100.00 %

5

Example 23  
Vegetable Oil Spread

Use the following procedure to prepare a vegetable oil spread.

Aqueous portion

10 Disperse Avicel®RC591F cellulose gel in available water  
 Add xanthan gum and allow 5 minutes for complete incorporation.  
 Incorporate the remaining aqueous portion and mix thoroughly for 10 minutes.  
 Heat the resulting aqueous mixture to 45-50°C (113°F-122°F).

15 Lipid portion

Heat the combined fats to 60°C (140°F) and hold at this temperature for 15 minutes.  
 In a small portion of the heated fats, melt the emulsifiers, bring the temperature to 80°C(176°F) and add back to the main portion of the fats.

20 Add fat soluble flavors and or colors. Cool the fat phase to 45-50°C(113°F-122°F).

- 42 -

Emulsification and crystallization

Add the aqueous portion to the lipid portion gradually under controlled mixing so as to obtain a uniform crude w/o emulsion, maintain a minimum temperature of 40°C(104°F).

- 5 Pass through a scraped surface chilling unit with an exit temperature of -15°C(59°F).

Table 14  
Aqueous Portion

10

Aqueous Portion	
% FAT	40%
Ingredients	%
Avicel ®RC591F cellulose gum	0.8
Xanthan gum	0.08
Salt	0.50
Potassium sorbate	0.2
Water to 100 %	to 100%
Color and flavor	to suit

Table 15  
Lipid Portion

Lipid Portion		
% Fat	40	40
Ingredients	%	%
Soya oil	20	20
Hydrogenated Soya Oil	11.64	11.64
Refined Palm Oil	7.9	6.50
Distilled monoglyceride	0.35	0.00
Composite	0.00	1.75
Flavor	to suit	to suit

- 15 Preferred ingredients:

Avicel®RC591 cellulose gum. Avicel is a trademark of FMC Corporation

- 43 -

Composite a 80/20 w/w microcrystalline cellulose/Dimodan mono and diglycerides, a product of Grinsted Products, which has an HLB of 3.0.

Example 24

Lowfat Frozen Desert

Prepare a lowfat frozen desert as follows:

Dairy mix procedure:

1. Assemble all liquid ingredients (cream, whole milk, condensed skim milk, liquid sweeteners) in a vat, then heat with agitation.
- 10 2. Dry blend powdered sweeteners, stabilizers, and emulsifiers. Add slowly to the liquid ingredients under good agitation. Mix 30 minutes to allow for dispersion and hydration of ingredients.
3. Pasteurize the mixture.
- 15 4. Homogenize the mixture, using a two stage pasteurizer, at 13790 kPa (2,000 pounds per square inch) (first stage) and 3447 kPa (500 pounds per square inch) (second stage).
5. Cool the mixture rapidly to 5°C (40°F). Age and mix overnight, if desired.
- 20 6. Freeze the mixture to an appropriate draw temperature, usually between -7.2°C and -5.6°C (19°F and 22°F), pack the mixture in containers, and place it in a hardening room.

25

30

35

- 44 -

Table 16  
Low Fat Frozen Desert

Ingredients	% Solids	% Solids
Butterfat	4.00	4.00
Milk solids nonfat	12.50	12.50
Sucrose	11.00	11.00
Corn Syrup Solids	5.00	4.30
Avicel®RC5811	0.40	0.40
cellulose gel		
Composite	0.00	1.00
Cellulose gum	0.10	0.10
Carrageenan	0.01	0.01
Emulsifier	0.30	0.00
Total Solids	33.31	33.31

Preferred ingredients:

5      Composite is a particle with a median size of approximately 15 to 20 micron that is an 80/20 w/w Avicel FD008 microcrystalline cellulose, a product of FMC corporation/Tandem 100 K a blend of mono and diglycerides and polysorbate 80, a product of Witco Corporation.

10

15

20

- 45 -

Claims

1. A food ingredient, characterized by:  
a cellulose composite having  
5        50 to 99% particulate cellulose based on the weight of the  
composite; and  
            1 to 50% surfactant coating, based on the weight of the  
composite, fixed to the cellulosic surface of the particulate cellulose,  
            characterized in that the surfactant used in the coating has an  
10     HLB within the range of from 7 to 25, and  
            characterized in that the cellulose composite has a mean particle  
size within the range of from 1 to 505 microns.
2. The cellulose composite of Claim 1,  
characterized in that:  
15     the cellulose composite has a mean particle size within the range  
of from 1 to 100 microns, and no more than 10 weight percent moisture,  
based on the weight of the composite;  
            the particulate cellulose represents 70 to 97 wt % of the  
composite; and  
20     the coating represents from 3 to 30 wt % of the composite; and  
            the surfactant used in the coating has an HLB within the range of  
from >10-25.
3. The cellulose composite of Claim 2, characterized in that:  
the particulate cellulose is 80 to 97 weight per cent of the  
25     composite; and  
            the coating is from 3 to 20 weight percent of the composite, and  
            the composite has a mean particle size within the range of from 1  
to 50 microns and contains no more than 6% moisture based on the weight  
of the composite.
4. The cellulose composite of Claim 3, characterized in that:  
the particulate cellulose is a microcrystalline cellulose, and  
30     the composite contains from 2 to 5 wt % moisture based on the  
weight of the composite.
5. The cellulose composite of Claim 4, characterized in that:  
35     the composite has a mean particle size within the range of from 5 to 30,

- 46 -

and an HLB within the range of >10 to 25.

6. The cellulose composite of Claim 4, characterized in that the composite has an HLB within the range of from 13 to 18.

7. A process for making a cellulose composite, characterized by  
5 coprocessing together a particulate cellulose of particle size between 1 and 500 micrometers, with a surfactant having a HLB within the range of >10 to 25 wherein the weight ratio of cellulose to surfactant ranges from 99:1 to 50:50.

8. The process of Claim 7, characterized in that coprocessing  
10 occurs under a high energy condition sufficient to drive the adsorption of the coating onto the surface of the particulate cellulose and dry the composite, thereby forming a dry, free flowing cellulose composite powder with a water content of less than 10% water.

9. The process of Claim 7, characterized in that coprocessing  
15 occurs, and further including a subsequent step of drying the composite until a substantially dry, free-flowing powder with a water content of less than 10% by weight is formed, based on the weight of the composite.

Claim 10. The process of Claim 9, characterized in that the  
coprocessed food ingredient has been dried until it has a water content  
20 within the range of 2 to 5 wt %.

11. The process of Claim 9 characterized in that the surfactant in the coating has an HLB within the range of from >10 to 25.

12. The process of Claim 9 characterized in that the surfactant in the coating has an HLB within the range of from 13 to 18.

25 13. The cellulose composite of Claim 3 characterized in that the coating includes one or more of the following: a fractionated lecithin, a monoglyceride, a diglyceride; an acetyl, lactyl, ethoxyl, succinyl, or diacetyl tartaric ester of a mono- and or a di- glyceride; a polyglycerol ester, a propylene glycol ester, a sorbitan ester, and a sucrose ester; a fat, an oil  
30 and other lipid materials.

14. The cellulose composite of Claim 13 characterized in that the coating includes a polyoxyethylene sorbitan ester.

15. A reduced calorie, food product characterized by:  
a food selected from one or more of the following: a pudding, a  
35 bread, a cake, a syrup phase confection, a margarine, a salad dressing, a

- 47 -

non-dairy creamer, a frozen dessert, a processed meat, an extruded snack; or a whipped dessert having the cellulose composite of Claim 2 dispersed therein,

characterized in that the food includes 1 to 35 wt % cellulose  
5 composite by weight of the food.

16. The use of the composite of Claim 3 as a bulking agent, as a texturizer, as a processing agent, or as a stabilizer.

17. The extruded snack of Claim 15, including a potato chip, corn  
curls, cheese puffs, french fries.

10

15

20

25

30

35

## INTERNATIONAL SEARCH REPORT

International application No. PCT/US95/01001
-------------------------------------------------

**A. CLASSIFICATION OF SUBJECT MATTER**

IPC(6) : A23L 1/308

US CL : 426/96

According to International Patent Classification (IPC) or to both national classification and IPC

**B. FIELDS SEARCHED**

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 426/96

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

**C. DOCUMENTS CONSIDERED TO BE RELEVANT**

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X ----- Y	US, A, 5,192,569 (MCGINLEY ET AL) 09 March 1993, col. 1, lines 36-40, col. 6, lines 51-54, col. 7, lines 2-9, col. 8, lines 12-14, col. 9, line 35.	1-16 ----- 17
X,P	US, A, 5,356,644 (HENDRICK ET AL) 18 October 1994, col. 2, lines 9-12, 39-43, 47-49, 50-52, 64-68, col. 3, lines 1-7, 19-22.	1-17

Further documents are listed in the continuation of Box C.  See patent family annex.

* Special categories of cited documents:	"T"	later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
*'A' document defining the general state of the art which is not considered to be of particular relevance	"X"	document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
*'E' earlier document published on or after the international filing date	"Y"	document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
*'L' document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reasons (as specified)	"Z"	document member of the same patent family
*'O' document referring to an oral disclosure, use, exhibition or other means		
*'P' document published prior to the international filing date but later than the priority date claimed		

Date of the actual completion of the international search  02 MARCH 1995	Date of mailing of the international search report  29 MAR 1995
--------------------------------------------------------------------------------	-----------------------------------------------------------------------

Name and mailing address of the ISA/US Commissioner of Patents and Trademarks Box PCT Washington, D.C. 20231 Facsimile No. (703) 305-3230	Authorized officer <i>Debbie Monroe</i> DONALD CZAJA <i>JTM</i> Telephone No. (703) 305-9646
-------------------------------------------------------------------------------------------------------------------------------------------------------	----------------------------------------------------------------------------------------------------